



# Linear Active Disturbance Rejection Control Using Plant Inverse Property

Tetsunori Koga and Ryo Tanaka

**Abstract:** In this paper, we propose a control law in a linear active disturbance rejection control (LADRC) for removal of ramp disturbance. We use plant inverse characteristics as a control law. We calculate the steady-state error of the conventional method and that of the proposed method using the final-value theorem. In a conventional and a proposed LADRC, each plant output has no steady-state error when a step signal is assumed as a plant input-side disturbance. However, in a conventional LADRC, the plant output has a steady-state error when a ramp signal is assumed as a plant input-side disturbance. On the other hand, in a proposed method, the plant output has no steady-state error. In comparison with a conventional method, the proposed method has almost the same control performance for a plant with a modeling error.

**Keywords:** Active disturbance rejection control. Extended state observer. Steady-state error. Plant inverse characteristics.

## I. INTRODUCTION

The origin of an active disturbance rejection control (ADRC) is a controller proposed by Han *et al* [1], [2]. By designing an extended state observer (ESO), unknown dynamics for plant model uncertainty and disturbances are estimated as a generalized disturbance. ADRC can compensate by estimating state variables and disturbance in real time and feeding back it [1], [3-5]. ADRC can control for not only a nonlinear mathematical model of a plant, but also a linear one. However, the structure of ADRC is complicated and there are many adjustment parameters. Therefore, linear version of ADRC (LADRC) has been proposed [4], [6], [7]. LADRC is composed of a linear ESO and a linear state feedback. Since LADRC has only two adjustment parameters, observer bandwidth  $\omega_o$  and controller bandwidth  $\omega_c$ , it is easy to tune.

Most of the papers about ADRC assume a step signal as a load disturbance. However, papers of ADRC concerning the ramp disturbance are few. Examples of a ramp disturbance are flow quantity change of the oil in the petrochemical plant and viscous frictional force when an equipment moves at uniform acceleration [8], [9]. It is essential to adapt such disturbances. In a conventional LADRC, the plant output has a steady-state error when a ramp disturbance is inserted.

To solve this problem, we propose a method to

reduce an influence of the ramp disturbance by changing the control law. We use plant inverse property as a control law. The proposed method rejects not only step disturbance but also ramp disturbance. The steady-state error of the proposed method and that of the conventional method are calculated by the final-value theorem. In comparison with a conventional method, the proposed method has almost the same control performance for a plant with a modeling error.

## II. TWO FORMULATIONS

This section describes the design method of ADRC.

### A. Linear ADRC (LADRC)

In a linear time invariant (LTI) system, the plant transfer function  $G_p(s)$  is

$$G_p(s) = \frac{Y(s)}{U(s)} = \frac{\sum_{j=0}^m (b_j + \Delta b_j) s^j}{s^n + \sum_{i=0}^{n-1} (a_i + \Delta a_i) s^i} \quad (1)$$

where:

$U(s)$  is a Laplace transform of a plant input.

$Y(s)$  is a Laplace transform of a plant output.

$a_i (i = 0, 1, \dots, n-1)$  and  $b_j (j = 0, 1, \dots, m)$  are nominal plant parameters.

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$\Delta a_i (i = 0, 1, \dots, n-1)$  and  $\Delta b_j (j = 0, 1, \dots, m)$  are error parameters of  $a_i$  and  $b_j$  caused by the plant modeling error.

ADRC doesn't need the accurate model of the plant and the disturbance, but the relative order of  $G_p(s)$ , and its gain  $b := b_m$ . The inverse Laplace transform in (1) is calculated by

$$y^{(p)}(t) = f(t) + \tilde{u}(t) \tag{2}$$

$$\tilde{u}(t) = bu(t) \tag{3}$$

where:

$f(t)$  is a total disturbance including the unknown dynamics and the external disturbance.

$p = n - m$  means a relative degree of a plant.

$y(t)$  is a plant output.

$y^{(p)}(t)$  is an  $p$ -th derivative of  $y(t)$ .

$u(t)$  is a plant input.

State variables  $x_i(t) (i = 1, 2, \dots, n+1)$  are defined as

$$\begin{cases} x_1(t) = y(t) \\ x_2(t) = \dot{y}(t) \\ \vdots \\ x_p(t) = y^{(p-1)}(t) \\ x_{p+1}(t) = f(t) \end{cases} \tag{4}$$

The time derivative of (4) is

$$\begin{cases} \dot{x}_1(t) = x_2(t) \\ \dot{x}_2(t) = x_3(t) \\ \vdots \\ \dot{x}_p(t) = y^{(p)}(t) = x_{p+1}(t) + \tilde{u}(t) \\ \dot{x}_{p+1}(t) = \dot{f}(t) \end{cases} \tag{5}$$

The matrix form in (4) and (5) is

$$\begin{cases} \dot{\mathbf{x}}(t) = \mathbf{A}_e \mathbf{x}(t) + \mathbf{B}_e \tilde{u}(t) + \mathbf{E} \dot{f}(t) \\ y(t) = \mathbf{C}_e \mathbf{x}(t) \end{cases} \tag{6}$$

where:

$$\mathbf{x}(t) = [x_1(t) \ x_2(t) \ \dots \ x_p(t) \ x_{p+1}(t)]_{<p+1> \times 1}^T$$

$$\mathbf{A}_e = \begin{bmatrix} 0 & 1 & 0 & \dots & 0 \\ 0 & 0 & 1 & \dots & 0 \\ \vdots & \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & 0 & \dots & 1 \\ 0 & 0 & 0 & \dots & 0 \end{bmatrix}_{<p+1> \times <p+1>}$$

$$\mathbf{B}_e = [0 \ 0 \ \dots \ 1 \ 0]_{<p+1> \times 1}^T$$

$$\mathbf{C}_e = [1 \ 0 \ \dots \ 0]_{1 \times <p+1>}$$

$$\mathbf{E} = [0 \ 0 \ \dots \ 0 \ 1]_{<p+1> \times 1}^T \tag{7}$$

The  $p+1$ -th order ESO for (7) is

$$\begin{cases} \dot{\hat{\mathbf{x}}}(t) = \mathbf{A}_e \hat{\mathbf{x}}(t) + \mathbf{B}_e \tilde{u}(t) + \mathbf{L} \{y(t) - \hat{y}(t)\} \\ \hat{y}(t) = \mathbf{C}_e \hat{\mathbf{x}}(t) \end{cases} \tag{8}$$

where:

$\hat{\mathbf{x}}(t)$  is an estimated state vector.

$\mathbf{L}$  is an observer gain vector.

$\hat{y}(t)$  is an estimated plant output.

Here,  $\mathbf{L}$  can generally be determined by a pole placement method, so that the eigenvalues of  $\mathbf{A}_e - \mathbf{L}\mathbf{C}_e$  are  $-\omega_o$ .

The block diagram of a linear ADRC is shown in Fig. 1.

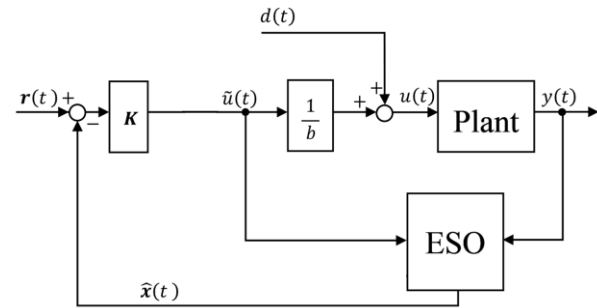


Fig. 1 Structure of LADRC

The control law is represented by

$$u(t) = \frac{\mathbf{K} \{r(t) - \hat{\mathbf{x}}(t)\}}{b} \tag{9}$$

where:

$$\mathbf{K} = [k_1 \ k_2 \ \dots \ k_p \ 1]$$

$$\mathbf{r}(t) = [r(t) \dot{r}(t) \dots r^{(p-1)}(t) r^{(p)}]^\top .$$

$$k_i = {}_p C_i \omega_c^{p+1-i} (i = 1, 2, \dots, p) .$$

${}_p C_i$  is a binomial coefficient.

### B. Modified ADRC (MADRC)

If we use an inverse model for a plant  $G_{inv}(s)$  and  $p$  integrators substituting for  $1/b$ , modified control law is as described below.

$$U(s) = G_{inv}(s) \cdot \frac{1}{s^p} \cdot \tilde{U}(s) \quad (10)$$

where:

$1/s^p$  describes  $p$  integrators to satisfy a proper transfer function.

$G_{inv}(s)$  is given as

$$G_{inv}(s) = \frac{s^n + \sum_{i=0}^{n-1} a_i s^i}{\sum_{j=0}^m b_j s^j} \quad (11)$$

The block diagram of the modified ADRC is shown in Fig. 2.

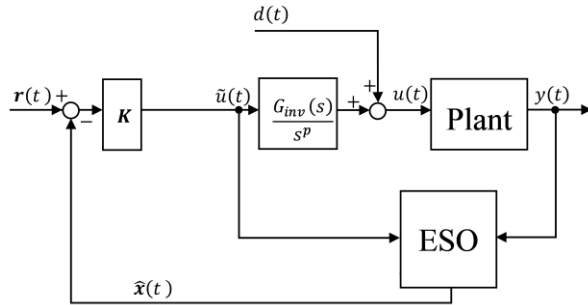


Fig. 2 Structure of MADRC

From Fig. 1 and Fig. 2, the Laplace transform of an input  $u(t)$  is

$$U(s) = \frac{\mathbf{K} \{ \mathbf{R}(s) - \hat{\mathbf{X}}(s) \}}{C(s)} + D(s) \quad (12)$$

where:

$$\mathbf{R}(s) = [1 \ s \ \dots \ s^{p-1} \ 0]^\top \mathbf{R}(s) .$$

$\mathbf{R}(s)$  is the Laplace transform of the reference signal  $r(t)$ .

$D(s)$  is the Laplace transform of an input-side disturbance  $d(t)$ .

If you use the LADRC,  $C(s) = b$ . If you use the MADRC,  $C(s) = s^p / G_{inv}(s)$ .

Arranging (8) and solving it for  $\hat{\mathbf{X}}(s)$ , we get

$$\begin{aligned} \hat{\mathbf{X}}(s) = & \{ s\mathbf{I}_{p+1} - \mathbf{A}_e + \mathbf{B}_e \mathbf{K} + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) \\ & + \mathbf{LC}_e \}^{-1} [ \{ \mathbf{B}_e \mathbf{K} + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) \} \mathbf{R}(s) \\ & + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BD}(s) ] , \end{aligned} \quad (13)$$

where:

$\mathbf{I}_n$  is an identity matrix of the  $n$  dimension.

From Fig. 1 and Fig. 2,  $Y(s)$  can be described as

$$Y(s) = C(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{B} \left[ \mathbf{K} \{ \mathbf{R}(s) - \hat{\mathbf{X}}(s) \} / C(s) + D(s) \right] . \quad (14)$$

By substituting (13) to (14),  $Y(s)$  can be described as

$$Y(s) = P(s)\mathbf{R}(s) + P_d(s)D(s) \quad (15)$$

where:

$$\begin{aligned} P(s) = & C(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) - C(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} \\ & \{ s\mathbf{I}_{p+1} - \mathbf{A}_e + \mathbf{B}_e \mathbf{K} + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) \\ & + \mathbf{LC}_e \}^{-1} \{ \mathbf{B}_e \mathbf{K} + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) \} . \end{aligned} \quad (16)$$

$$\begin{aligned} P_d(s) = & C(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{B} - C(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} \\ & (s\mathbf{I}_{p+1} - \mathbf{A}_e + \mathbf{B}_e \mathbf{K} + \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{BK} / C(s) \\ & + \mathbf{LC}_e)^{-1} \mathbf{LC}(s\mathbf{I}_n - \mathbf{A})^{-1} \mathbf{B} . \end{aligned} \quad (17)$$

By using the final-value theorem, we calculate the steady-state error  $e_{ss}$  as shown below

$$e_{ss} = \lim_{t \rightarrow \infty} e(t) = \lim_{s \rightarrow 0} sE(s) \quad (18)$$

where:

$$e(t) = r(t) - y(t).$$

The Laplace transform of  $e(t)$  is described as

$$E(s) = R(s) - Y(s) = (1 - P(s))R(s) - P_d(s)D(s).$$

$R(s)$  is the Laplace transform  $1/s$  of a unit step input

$D(s)$  is the Laplace transform  $k_s/s$  of a step disturbance or  $k_r/s^2$  of a ramp disturbance.

$k_s$  is a magnitude of the step disturbance.

$k_r$  is a magnitude of the ramp disturbance. Then,  $e_{ss}$  is summarized as shown in table.1.

**Table.1** Steady-state error  $e_{ss}$

Relative order	LADRC	MADRC
1	$\frac{k_r c(\omega_c + 2\omega_o)}{\omega_c \omega_o^2}$	0
2	$\frac{k_r c(\omega_c^2 + 6\omega_c \omega_o + 3\omega_o^2)}{\omega_c^2 \omega_o^3}$	0
3	$\frac{k_r c(\omega_c^3 + 12\omega_c^2 \omega_o + 18\omega_c \omega_o^2 + 4\omega_o^3)}{\omega_c^3 \omega_o^4}$	0

### III. SIMULATIONS

#### A. Simulations Setups

We performed simulations for five kinds of plants.

When the plant is a nominal model,  $(\Delta b_2, \Delta b_1, \Delta b_0, \Delta a_2, \Delta a_1, \Delta a_0) = (0, 0, 0, 0, 0, 0)$ .

If the plant has a modeling error, we assume that  $(\Delta b_2, \Delta b_1, \Delta b_0, \Delta a_2, \Delta a_1, \Delta a_0) = (0.5b_2, 0.5b_1, 0.5b_0, 0.5a_2, 0.5a_1, 0.5a_0)$ .

In simulation,  $(\omega_o, \omega_c, k_s, k_r) = (50, 10, 1, 1)$ . A unit step signal and a unit ramp signal are assumed as a plant input-side disturbance. One of these disturbances is loaded at eight seconds.

$$\text{plant1: } G_p(s) = \frac{50s + 200}{s^2 + 11s + 10}$$

$$\text{plant2: } G_p(s) = \frac{175s^2 + 525s + 350}{s^3 + 10s^2 + 29s + 20}$$

$$\text{plant3: } G_p(s) = \frac{340}{s^2 + 11s + 10}$$

$$\text{plant4: } G_p(s) = \frac{50s + 200}{s^3 + 10s^2 + 29s + 20}$$

$$\text{plant5: } G_p(s) = \frac{200}{s^3 + 10s^2 + 29s + 20}$$

#### B. Simulation Results

From Figs. 3 to 12 show simulation results of output responses. As shown in these results, both methods have superior robustness for the plant with a modeling error. From Figs. 3, 5, 7, 9 and 11, in LADRC and MADRC, each plant output has no steady-state error when a step signal is assumed as a plant input-side disturbance. From Figs. 4, 6, 8, 10 and 12, in LADRC, the plant output has a steady-state error when a ramp signal is assumed as a plant input-side disturbance. On the other hand, in MADRC, the plant output has no steady-state error.

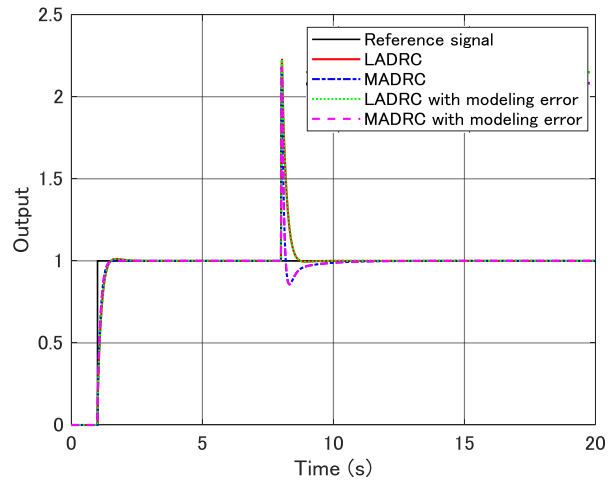


Fig. 3 Output of plant1 (step disturbance)

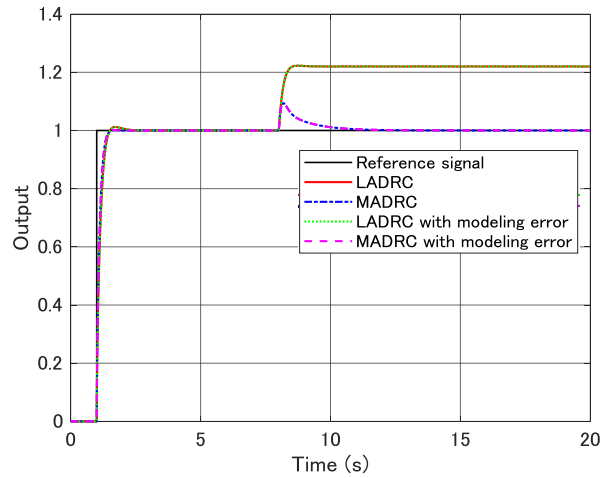


Fig. 4 Output of plant1 (ramp disturbance)

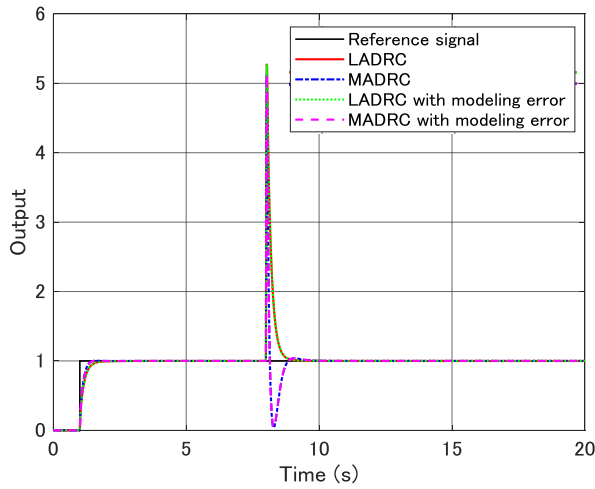


Fig. 5 Output of plant2 (step disturbance)

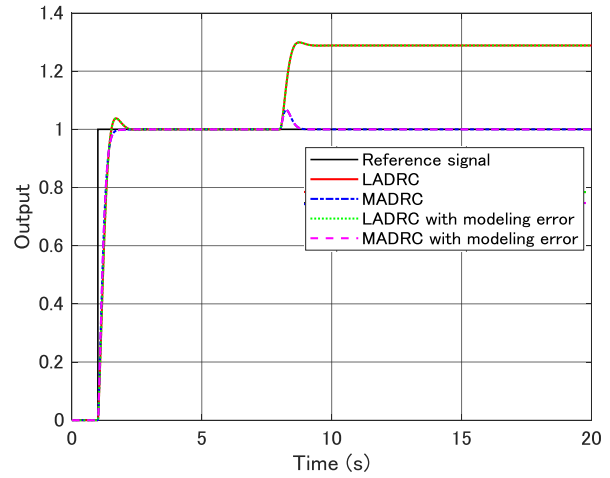


Fig. 8 Output of plant3 (ramp disturbance)

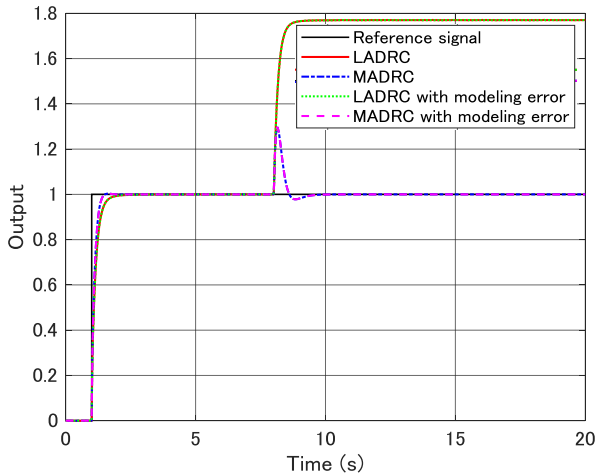


Fig. 6 Output of plant2 (ramp disturbance)

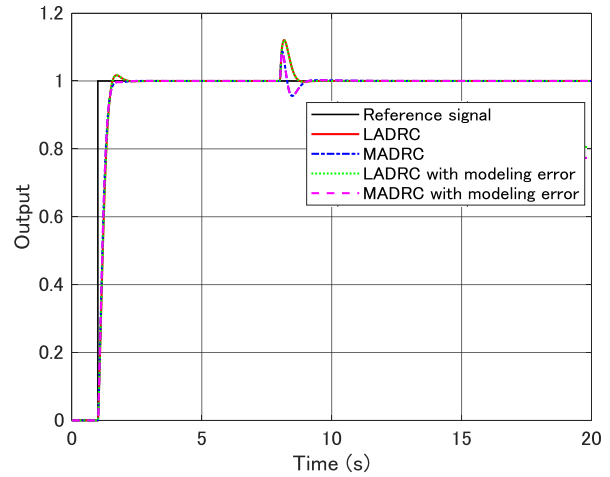


Fig. 9 Output of plant4 (step disturbance)

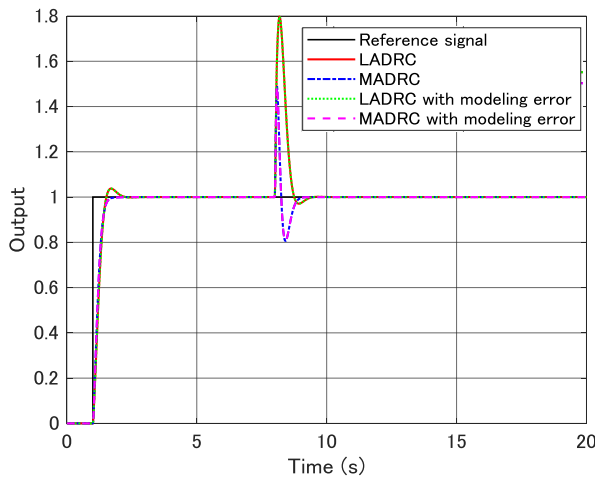


Fig. 7 Output of plant3 (step disturbance)

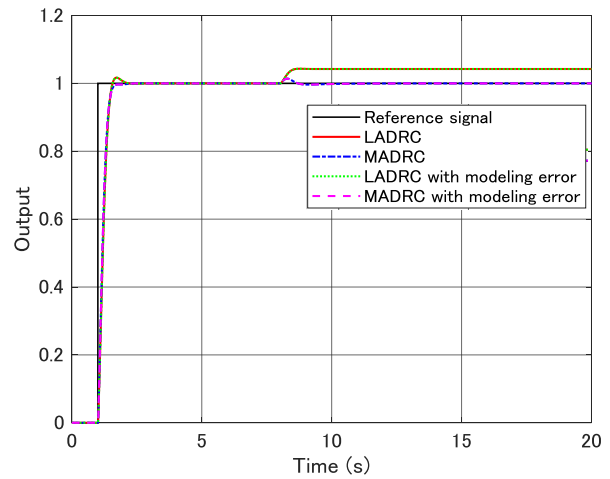


Fig. 10 Output of plant4 (ramp disturbance)

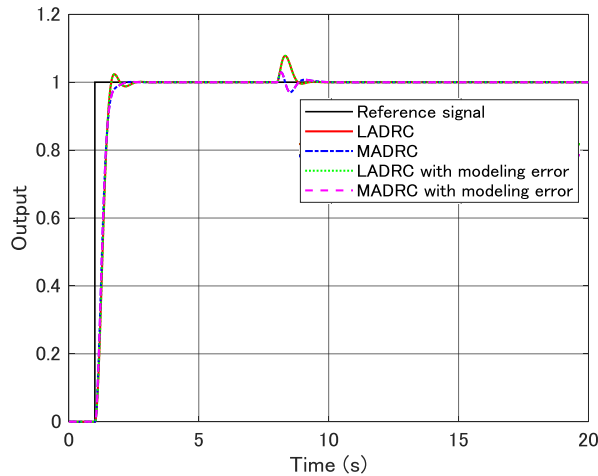


Fig. 11 Output of plant5 (step disturbance)

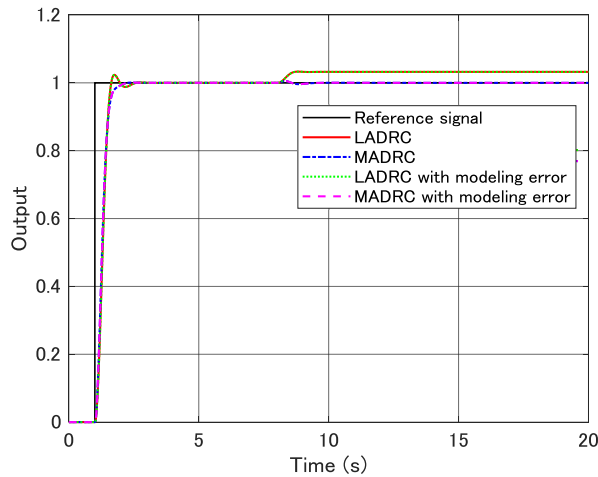


Fig. 12 Output of plant5 (ramp disturbance)

#### IV. CONCLUSIONS

We have proposed a modified control law in ADRC. We also have proved that steady-state error is zero using the final-value theorem. In simulations, we have confirmed that the proposed method has an excellent robustness for a plant with a modeling error.

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